INTEGRATED SOLUTIONS FOR SUGAR PLANT CONSTRUCTION & MODERNIZATION

HEAT AND MASS TRANSFER EQUIPMENT



Volodymyr-Volynsky Sugar Plant, Gaisyn Sugar Plant, Naumivka Ethanol Plant, Babyno-Tomakhivsk Sugar Plant, Ivashky Ethanol Plant, Trylisy Ethanol Plant, Korostyshiv Ethanol Plant

Olhovatsky Sugar Factory, Nikiforovsky Sugar Plant, Zherdevka Sugar Plant

Skidel Sugar Factory

Stara Zagora

Kaindy-Kant Sugar Plant

Nordzucker Group

Techinservice

References:

UKRAINE

RUSSIA		
BELARUS		
1.200	C.S.	
BULGARIA		
	Contract of	
KYRGYZSTAN		
GERMANY		

H E A T A N D M A S S T R A N S F E R E Q U I P M E N T

MODERN VACUUM CONDENSING UNITS OF SUGAR PLANTS

Vacuum condensing units (VCU) are designed for maintaining a constant operating pressure in the sugar factory's vacuum system.

Techinservice designs and constructs VCU equipment and schemes providing all the advantages in condenser design.

The **Techinservice** vacuum condensing units include the following equipment:

- raw juice heaters (surface condensers);
- condensers;
- cooling towers;
- VCU automatic control system.



Vacuum Condensing Unit at Volodymyr-Volynsky Sugar Plant

RAW JUICE HEATERS (SURFACE CONDENSERS)

The VCU has two groups of heaters for heating raw juice with crystallization vapors, namely:

1st group – B and C product crystallization vapors;

2nd group – A product crystallization vapors and secondary steam from the last effect of evaporation station.

Vapor is fed into the shell section of the heater, where some of this vapor is condensed. Raw juice is heated nearly up to the condensable vapor temperature of $\Delta t = 1-2$ °C. This allows using secondary energy resources more effectively and reducing the exhaust steam consumption necessary for production of sugar. The pressure drop in the heater as well as in the VCU scheme developed by **Techinservice** is compensated in the condenser designed by **Techinservice** (the pressure drop in the steam flow does not exceed 1.5 kPa).

Such design solution allows:

- using the total volume of crystallization vapors to be condensed for heating raw juice;
- maintaining a constant operating pressure in the sugar factory's vacuum system;
- decreasing the flow rate of vapor fed into the condenser by the flow rate of vapor condensed in the heater;
- reducing the cooling water consumption.



Shipment of Raw Juice Heater at Grebinky Machine-Building Plant

Operating parameters of the raw juice heater installed at the **Nordzucker AG** sugar plant: 850 m³ of juice per hour is heated from 18 up to 40 °C with crystallization vapors having the temperature of 53 °C. And the vapor flow rate condensed is 37 t/h.



Raw Juice Heater Mounted at the Uelzen Nordzucker Refinery





Vacuum Condensing Unit (Vertical Arrangement)

CONDENSERS

The condensers constructed by **Techinservice** are based on the principle of intensive mass heat exchange achieved due to fine liquid atomization.

Main technical and economic features of **Techinservice** condensers:

• pressure drop in the steam flow does not exceed 1.5 kPa (150 mm w.g.);

• possibility to heat process water nearly up to the condensable vapor saturation temperature $[\Delta t_{subcooling 1} = 0.3-0.7 \degree C];$

• possibility to heat cooling water in the condensation zone of bulk vapor ($\Delta t_{subcooling 2} = 0.7-2.5 \text{ °C}$);

• reliable operation and hydrodynamic stability;

• lower content of metal in structure.

The performance of these condensers is not affected by sharp fluctuations of the vapor flow rate as well as the cooling water temperature. These condensers' advantages are the result of their original structural design.



The Techinservice condensers can be manufactured in a vertical or horizontal design:

MODULE 1

for heating fresh water required for process needs

MODULE 2

for maintaining vacuum in A-product vacuum pans at 0.8-0.84 kg/cm²

MODULE 3

for maintaining vacuum in B & C-product vacuum pans at 0.9-0.99 kg/cm²



H E A T M A N D M A S S T R A N S F E R M E Q U I P M E N T



Raw Juice Heater (PDU) at Clauen Nordzucker Sugar Plant



VCU Technical Specification				
Model	Capacity on condensable vapour, t/hour	Pressure drop, mm w.g.		
K-6	6			
K-17	17			
K-20	20			
K-20M1	20			
K-25	25			
K-45	45			
K-50	50			
K-60	60			
K-75	75			
S-6	6			
S-10	10			
S-12	12			
S-25	25			
S-30	30	153		
S-35	35			
S-40	40			
TKK-3.5 (combined A and B+C products)	AA product – 25 t/h, B+C products – 10 t/h			
TKK-6 (combined A and B+C products)	A product – 40 t/h, B+C products – 15 t/h			
TKC-1A	0.02			
TKC-3A	0.025			
TKC-4	4			
TKC-5	5			
TKC-20	20			
TKC-40	40			

AUTOMATIC CONTROL SYSTEM

The main feature of the vacuum condensing unit control system is the use of several valves feeding water to the condenser, which open/close depending on the vacuum level as well as the temperature of incondensable gases and outlet cooling water, which allows minimizing the cooling water consumption.

If the VCU control system is used simultaneously with the sugar end control system, when a vacuum pan is started or stopped, the water feed is automatically changed slightly for preventative adjustment of vacuum in the collector.

VCU Operation Field Case				
Parameter	2 nd Group Heater + A-Product Condenser	1 st Group Heater + B&C-Product Condenser		
Vapor flow rate, t/h	20÷75	7÷20		
Absolute vapor pressure, MPa	0.02÷0.017	0.01÷0.014		
Inlet fresh water temperature, °C	4÷20	-		
Inlet raw juice temperature, °C	43	27		
Outlet raw juice temperature, °C	58÷59	43		
Outlet fresh water, °C	58÷60	-		
Inlet cooling temperature, °C	30	30		
Incondensable gases temperature, °C	32	32		
Pressure drop in the steam flow, kPa	not more than 1.5	not more than 1.5		



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